

In Situ Geochemical Stabilization (ISGS) for NAPL Management

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Presentation Overview

- What is ISGS Technology?
- History of ISGS Technology
- Proof of Concept / Bench Testing
- Field Applications
 Denver, CO
 Gainesville, FL
 Fanwood, NJ
 Boston, MA
- Geochemical Modeling related to Permanence/Longevity
- Costs
- Questions?



Contaminant Flux Definition (Enfield, 2001)



ISGS™ Chemistry



ISGS solution is a proprietary blend of permanganate and mineral salts that form a stable mineral precipitate



In the presence of an organic compound (R), MnO4 reactions yield an oxidized intermediate (Rox) or CO2 ,... plus MnO2

 $R + MnO_4 - \rightarrow MnO_2 + CO_2 \text{ or Rox}$

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ISGS™ Chemistry

Reagent Composition:

> Modified permanganate solution

Proprietary combination of cold-water soluble inorganic metals & salts which serve as hardening or concretizing agents

• Mechanisms of Action:

> Permanganate reacts with dissolved phase organic contaminants:

- ✓ "Hardening" or "chemical weathering" of residual NAPL
- MnO2 generated preferentially in high concentration area surrounding NAPL
- Proprietary reagents react with MnO2 to form a stable precipitate

> Precipitate rapidly reduces porosity (>80%) and permeability (>90%)

mass removal + reduced NAPL mobility

+ reduced porosity = flux reduction (i.e., long-term NAPL stabilization)





A New NAPL Management Tool



ISGS Effects
 Creates a stable "crust"
 Reduces permeability
 Immobilizes NAPL



ISGS Addresses NAPL Challenges

- Reduces measurable NAPL
- Reduces dissolution of NAPL constituents
- Reduces flux of NAPL into groundwater
- Scheme Sc



- 1. Liquid amendment easy to inject and target source areas.
- 2. Rapid reactions (days) yield reduced aquifer permeability and COI flux
- 3. Applicable to wide range of organic and inorganic COIs
- 4. Only treat a fraction of TOD
- Long term (crust analyses & geochemical modeling suggest > 100 yr, supported by over 10 yr field data)
- 6. Relatively low cost for localized source areas
- 7. Logical alternative to mass removal and mass destruction





Technology Development



- 1997 Conceptualization / Proof of Concept
- 3 1998 1999 TCE R&D at UW and Adventus
- 3 1999 2001 Camp Borden (pilot)
- 3 2002 2003 PAHs, PCP Denver, CO (pilot)
- C3 2004 PAHs Denver, CO (full scale)
- 3 2004 PAHs, PCP Gainesville, FL (bench).
- 3 2005 PAHs, PCP Gainesville, FL (pilot)
- 3 2007 PAHs MGP NE Utilities (bench)
- 3 2008 PAHs, PCP Gainesville, FL (pilot)
- 3 2008 PAHs Creosote works, LA (bench)
- 3 2009 solvents, benzene plastics manufacturer (bench)
- 3 2010 PAHs Montgomery, AL (full scale)
- 3 2010 LNAPL South Boston, MA (bench test)
- 3 2013 LNAPL Fanwood, NJ (full-scale)
- C3 2013 LNAPL and DNAPL, Frankford, PA (pilot test)
- 3 2013 Creosote and PAHs Gainesville (full scale)
- 3 2013 Coal Tar and PAHs Fanwood, NJ

Proof of Concept- Bench Testing



Saturate w/ISGS reagents

C320 days reaction time

SDrain

Compare with Control

Typical Bench Test Results – COIs in Leachate (ca. 7 days treatment time)



First Full-Scale Application - Denver, CO (3) PeroxyChem



Pre Injection – NAPL Thickness (ft)



Post Injection – NAPL Thickness (ft)





Non-Treated Soil 14 ft bgs

ISGS Treated Soil 14 ft bgs



ISGS [™] - Case Study Koppers Site, Denver, CO



Site: Former Kopper's Inc Superfund Site, CO

Application: 24,050 USG of 3% ISGS solution injected into 13 locations target area = 75 ft x 95 ft x 10 ft

Mass Removal:

COI (mg/kg)	Average (n=4) Background	Average (n=4) Treated	% Reduction
LMW PAHS	7,633.50	5,996.75	21
HMW PAHs	1,961.55	1,744.55	10
TOTAL PAHs	9,595.05	7,771.30	19
* PENTA	236.00	55.67	76
* TOTAL CPs	284.48	59.25	79

Flux Reduction:

COI (mg/L)	Average Background	Average Treated	% Reduction
LMW PAHS	34.41	12.75	73
HMW PAHs	6.05	0.11	99
TOTAL PAHs	40.46	12.86	79
* PENTA	18.91	9.66	49
* TOTAL CPs	23.38	10.41	56

Phase II ISGS Application (2004)



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Fanwood, NJ Site

- Historical release of coal tars and heavy ended petroleum compounds.
- The COCs included benzene, naphthalene,
 Benzo(a)anthracene, Benzo(a)pyrene, and multiple other
 VOCs and SVOCs.
- The in-situ program covered a total area of 8,955 square feet and treated soil and groundwater from 5-10 ft. below ground surface.
- ISGS solution were injected into 44 points via direct push technologies.
- Two intervals between from 5-7 and 8-10 feet below ground surface (bgs) were used to inject the liquids into the targeted media affecting a radius of 7.5 feet for each point.



Five monitoring wells were sampled during the baseline sampling event of August 2013 and the first two post-injection sampling events. These wells are: MW-11, MW-12, MW-13, MW-14 and MW-15.

Tuble I. e. e e Duta for Mr. II (µg.L).				
MW-11				
Sampling Date	08/30/2013	10/16/2013	01/15/2014	
Acenaphtylene	0.461	0.312	ND 0.10	
Benzo(a)anthracene	0.255	0.847	0.146	
Benzo(a)pyrene	0.172	0.54	ND 0.10	
Benzo(b)fluoranthene	0.218	0.76	ND 0.10	
Chrysene	0.166	0.508	ND 0.10	
Fluorene	0.791	0.314	0.239	
Benzene	67.5	8.4	14.4	
Ethylbenzene	6.6	ND 5.0	0.77 J	
Toluene	46.5	ND 5.0	3.0	
Total Xylenes	19.1	ND 5.0	2.7	
Total Alkanes	63 J	ND	ND	

Table 1. CVOC Data for MW-11 (µg/L).





Table 3. CVOC Data for MW-13 (µg/L).

MW-13				
Sampling Date	08/30/2013	10/16/2013	01/15/2014	
Acenaphtylene	81.3	11.6	0.64	
Benzo(a)anthracene	2.92	0.435	0.684	
Benzo(a)pyrene	1.75	ND 0.10	0.192	
Benzo(b)fluoranthene	2.24	ND 0.10	0.233	
Benzo(g,h,i)perylene	0.698	ND 0.10	ND 0.10	
Benzo(k)fluoranthene	0.895	ND 0.10	0.121	
Chrysene	2.02	0.235	0.409	
Naphthalene	1,920	187	1.18	
Benzene	100	48.7	175	
Ethylbenzene	43.4	10.4	61.9	
Toluene	160	24.4	161	
Total Xylenes	179	41.6	171	
Total Alkanes	3,625 J	ND	ND	

Free Product Data

Ten different wells were sampled before the implementation of the remedial injection event of September 2013 and the depth of the free product that was present in each well was measured. As Table 6 shows all ten wells appear to have elevated free product levels during the March 2013 baseline sampling event that ranged from 1.22 ft to 5.37 ft.

	Sampling Date					
Well ID	05/25/2012	06/07/2012	03/14/2013	10/16/13	10/18/13	1/15/14
TW-1/MW-14	4.16	3.90	4.24	ND	ND	ND
TW-2/MW-15	5.34	4.98	5.31	ND	ND	ND
TW-3/MW-11	5.26	5.12	5.37	ND	ND	ND
TW-4	5.35	5.02	5.11			
TW-5/MW-12	5.60	4.99	4.64	ND	ND	ND
TW-6	4.06	4.02	3.75			
TW-7	5.31	5.08	5.11			
TW-8/MW-13	3.43	3.07	3.26	ND	ND	ND
TW-9	1.15	1.14	1.22			
TW-10	5.02	5.09	4.16			

Table 6. Injection Thickness of Free Product (ft).







South Boston Site – Bench Test







• Objectives:

- Solution Validate ISGS treatment applicability to TPH
- Identify most cost-effective treatment regime (based on site soil)
- Method:
 - batch & column studies
- Results:
 - CSTOD 5 to 8 g/kg (B-Header), 30 to 42 g/kg (WE-27)
 - cos 60 to 80% reduction in EPH leachate concentrations in 14 days
 - 3 13 to 30% reduction in EPH soil concentrations in 14 days
 - G 44 to 67% reduction in permeability to NAPL and 17% reduction in NAPL fluid saturation
 - ISGS was effective for NAPL stabilization for soils and constituents at this site
 - 4.5% ISGS solution was recommended for full-scale

Cabot Carbon / Koppers Superfund Site, Gainesville, FL





- •90 acre site
- Pump & treat in place
- Secondary NAPL issues



Results - NAPL Monitoring Wells





1 week Post ISGS treatment = no measurable free-phase NAPL in any of the monitoring wells.



Monitoring Well	Pre-Injection	Post-Injection
NISBS-1		stain
TIP-3	ND	ND
	ND	ND
UGH Recovery	NAPL	No NAPL

Results -Total PAH Concentrations in Soil and in Leachate



6 cores (3 sections) before treatment

PeroxyChem

6 cores (2 depths) after treatment

Best matched cores (SOIL): dropped from 7,250 mg/kg to 3,600 mg/kg

Best matched cores (LEACHATE): dropped from 11,700 mg/L to 560 mg/L

PAH concentrations in soil reduced by up to 50% within 3 months.

PAH leachate concentrations reduced by up to 98% within 3 months.

ISGS Field Data – Decrease in K_h Values Woodward Coke Site – Dolomite, AL





Treated Soil Core Close-up Showing ISGS "Crust" or Coating and NAPL Ganglia







Likely NAPL

ISGS coating

Soil Grain

Epoxy (open pore space)

Conclusion: Soil grains and NAPL blobs coated with ISGS crust

Birnessite is an oxide of Mn and Mg along with Na, Ca and K with the composition: (Na,Ca,K)(Mg,Mn)Mn₆O₁₄.5H₂O







Crust Longevity

Crust weathering is dependent on changes in Eh and pH
Conduct mineralogy assay
Validate using geochemical modeling

Performance Monitoring
 SEh, pH for crust stability
 Permeability tests for flux reduction
 NAPL fluid saturation

Geochemical Modeling of the Crust





Crust Longevity

- Back of the envelope calculations suggest crust life ~ 400 years.
- This may be over-estimated because it assumes Eh (-400 mV) and pH (6) at which birnessite is sparingly soluble



Figure 16. Fields of stability of manganese solids and equilibrium dissolved manganese activity as a function of Eh and pH at 25°C and 1 atmosphere pressure. Activity of sulfurspecies 96 mg/L as SO_1^2 , and carbon dioxide species 61 mg/L as HCO_3 .

Eh-pH diagram from Hem (1985)

Representative Experience ISGS – Creosote and Related Sites



Site	COI / Environmental Setting	ISGS Approach / Status
Active Wood Treating Site Superfund Site Denver, CO	Phase separated creosote (PAHs) and pentachlorophenol (penta). Consolidated shallow alluvium.	KMnO4 (no catalysts; no buffer) successful bench and pilot studies completed; full-scale application completed 2004.
(Active) Wood Treating Site Superfund Site Gainesville, FL	Phase separated creosote (PAHs). Sand silt environment, 5 to 22 ft bgs.	NaMnO4 (catalyzed, buffered) completed bench-scale engineering optimization tests; Pilot-scale technology validation performed in January 2008. 2012 Full- scale application recommended as part of the ROD – installation 2013 to 2015.
Former Wood Treating Site Montgomery, AL	Phase separated creosote (PAHs)	Field Scale application completed 2009. One to two orders of magnitude reduction in permeability.
Former Wood Treating Site Cape Fear, NC	Phase separated creosote (PAHs)	Conceptual design completed.
Former American Creosote Works Winnfield, LA	Phase separated creosote (PAHs)	Engineering optimization bench work completed.
Former Wood Treating Site Sand Point, ID	Phase separated creosote (PAHs)	Engineering optimization bench work completed; Field Pilot Completed Q3 2010.
Former Wood Treating Site Netherlands	Phase separated creosote (PAHs)	Engineering optimization bench work completed. Field Pilot pending

ISGS Material Cost – Field Applications

Denver, CO	Dolomite, AL	Gainesville, FL
TOD = 18 g/kg	TOD = 1 g/kg	TOD = 122 g/kg
Dense Alluvium KMnO ₄ @ 4.5 g/kg Injection Wells	Fractured Karst RemOx EC Push-Pull	Sand/Silt RemOx EC Direct Push and Injection wells
1,273 m ³ soil 3% solutions 1,850 USG/IP 2-5 gpm (20 psi)	1,500 m ³ soil 1% solutions 20,000 USG 13 gpm (20-50 psi)	1,415 m ³ soil 4.5 % solutions 620 USG/DIP 2-5 gpm (<50 psi)
Cost = \$40 - 50/m ³ \$31 - 38/yd ³	Cost = \$45 - 50/m ³ \$34 -38/yd ³	Cost = \$60 - 75/m ³ \$50 -60/yd ³

The amount of ISGS reagent required for a given site has a significant influence on project cost. Typical **material costs** range from \$13/yd³ to \$53/yd³.

Questions?